AMENDMENTS TO THE CLAIMS

We claim:

1. (currently amended) A process for obtaining oligomers of polytetrahydrofuran or of tetrahydrofuran copolymers from a methanolic crude product which contains polytetrahydrofuran or tetrahydrofuran copolymers and is obtained in the transesterification of the mono- and/or diesters of polytetrahydrofuran or tetrahydrofuran copolymers with methanol, which comprises:

   a) removing the majority of the methanol from the crude product in a first distillation stage[,] ;

   b) separating the resulting bottom product by distillation into a top fraction comprising the oligomers of polytetrahydrofuran or of tetrahydrofuran copolymers, and polytetrahydrofuran or tetrahydrofuran copolymer[,] ; and

   c) condensing the oligomers of polytetrahydrofuran or of tetrahydrofuran copolymers out of the top fraction from stage b).

2. (original) A process as claimed in claim 1, wherein the methanol removed in stage a) is recycled into the transesterification.

3. (currently amended) A process as claimed in ~~either of claims 1 and 2~~ claim 1, wherein distillation is effected in stage a) at from 20 to 500 mbar gauge and a temperature of from 50 to 250°C.

4. (currently amended) A process as claimed in ~~any of claims 1 to 3~~ claim 1, wherein distillation is effected in stage b) at an absolute pressure of from 1 to 300 mbar and at from 50 to 250°C.

5. (currently amended) A process as claimed in ~~any of claims 1 to 4~~ claim 1, wherein condensation is effected in stage c) at a temperature of from 5 to 40°C.

6. (currently amended) A process as claimed in ~~any of claims 1 to 5~~ claim 1, wherein the crude product obtained is freed before stage a) of sodium ions stemming from the transesterification catalyst by treatment with an ion exchanger.

7. (new) A process as claimed in claim 2, wherein distillation is effected in stage a) at from 20 to 500 mbar gauge and a temperature of from 50 to 250°C.

8. (new) A process as claimed in claim 2, wherein distillation is effected in stage b) at an absolute pressure of from 1 to 300 mbar and at from 50 to 250°C.

9. (new) A process as claimed in claim 3, wherein distillation is effected in stage b) at an absolute pressure of from 1 to 300 mbar and at from 50 to 250°C.

10. (new) A process as claimed in claim 2, wherein condensation is effected in stage c) at a temperature of from 5 to 40°C.

11. (new) A process as claimed in claim 3, wherein condensation is effected in stage c) at a temperature of from 5 to 40°C.

12. (new) A process as claimed in claim 4, wherein condensation is effected in stage c) at a temperature of from 5 to 40°C.

13. (new) A process as claimed in claim 2, wherein the crude product obtained is freed before stage a) of sodium ions stemming from the transesterification catalyst by treatment with an ion exchanger.

14. (new) A process as claimed in claim 3, wherein the crude product obtained is freed before stage a) of sodium ions stemming from the transesterification catalyst by treatment with an ion exchanger.

15. (new) A process as claimed in claim 4, wherein the crude product obtained is freed before stage a) of sodium ions stemming from the transesterification catalyst by treatment with an ion exchanger.

16. (new) A process as claimed in claim 5, wherein the crude product obtained is freed before stage a) of sodium ions stemming from the transesterification catalyst by treatment with an ion exchanger.